

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

REQUEST FOR FILING CONTINUATION/DIVISIONAL
APPLICATION UNDER 37 C.F.R. § 1.53(b)

Box PATENT APPLICATION
Assistant Commissioner for Patents
Washington, D.C. 20231

Sir:

This is a request for filing a ☐ continuation ☒ divisional application under 37 C.F.R.
§ 1.53(b) of pending Application No. 09/090,918 filed on June 5, 1998, for PROCESS FOR
REMOVING UNREACTED AMMONIA FROM AN EFFLUENT IN A HYDROCARBON
AMMOXIDATION REACTION, by the following named inventor(s):

- (a) Full Name Xin CHEN
(b) Full Name Lianghua WU
(c) Full Name _____

☒ The entire disclosure of the prior application from which a copy of the oath or declaration is
supplied herewith is considered as being part of the disclosure of the accompanying
application and is hereby incorporated by reference therein.

☐ This application is being filed by less than all the inventors named in the prior application.
In accordance with 37 C.F.R. 1.63(d)(2), the Commissioner is requested to delete the
name(s) of the following person or persons who are not inventors of the invention being
claimed in this application.

- (a) Full Name _____
(b) Full Name _____
(c) Full Name _____

☐ This application is being filed by more than all the inventors named in the prior application.
In accordance with 37 C.F.R. 1.63(d)(2), the Commissioner is requested to add the name(s)
of the following person or persons who are inventors of the invention being claimed in this
application.



21839

- (a) Full Name _____
(b) Full Name _____
(c) Full Name _____

1. ☒ Enclosed is a copy of the prior Application No. 09/090,918 as originally filed on June 5, 1998, including copies of the specification, claims, drawings and the executed oath or declaration as filed.
2. ☐ Enclosed is a revised prior application and a copy of the prior executed oath or declaration as filed. No new matter has been added to the revised application.
3. ☐ _____ statement(s) claiming small entity status ☐ are enclosed ☐ were filed in prior Application No. __, filed on __.
4. ☒ The filing fee is calculated below ☒ and in accordance with the enclosed preliminary amendment:

CLAIMS					
	NO. OF CLAIMS		EXTRA CLAIMS	RATE	FEE
Basic Application Fee					\$760.00 (101)
Total Claims	5	MINUS 20 =	0	x \$18.00 (103) =	0.00
Independent Claims	1	MINUS 3 =	0	x \$78.00 (102) =	0.00
If multiple dependent claims are presented, add \$260.00 (104)					
Total Application Fee					760.00
If small entity status is claimed, subtract 50% of Total Application Fee					
Add Assignment Recording Fee of if Assignment document is enclosed					
TOTAL APPLICATION FEE DUE					760.00

5. ☒ Charge \$ 760.00 to Deposit Account No. 02-4800 for the fee due.

6. ☐ A check in the amount of \$ _____ is enclosed for the fee due.
7. ☒ The Commissioner is hereby authorized to charge any appropriate fees under 37 C.F.R. §§ 1.16, 1.17 and 1.21 that may be required by this paper, and to credit any overpayment, to Deposit Account No. 02-4800. This paper is submitted in triplicate.
8. ☐ Cancel in this application original claims __ of the prior application before calculating the filing fee. (At least one original independent claim must be retained for filing purposes.)
9. ☒ Amend the specification by inserting before the first line the sentence: --This application is a ☐ continuation, ☒ divisional, of Application No. 09/090,918, filed June 5, 1998.--
10. ☐ Transfer the drawings from the pending prior application to this application and abandon said prior application as of the filing date accorded this application. A duplicate of this paper is enclosed for filing in the prior application file. (May only be used if signed by person authorized under 37 C.F.R. § 1.138 and before payment of issue fee.)
11. ☐ New drawings are enclosed.
12. ☒ Priority of Application No. CN97106455.5 filed on June 6, 1997 in China (country) is claimed under 35 U.S.C. § 119.
- ☒ The certified copy of the priority application
☐ is enclosed
☒ was filed on September 17, 1998 in prior Application No. 09/090,918, filed on June 5, 1998
☐ has not yet been filed.
13. ☒ A preliminary amendment is enclosed.
14. ☒ A General Authorization for Payment of Fees and Petitions for Extensions of Time.
15. ☒ Also enclosed is a substitute Abstract.
16. ☒ The power of attorney in the prior application is to William C. Rowland and all other partners of Burns, Doane, Swecker & Mathis, L.L.P..
- a. ☒ The power appears in the original papers in the prior application.
- b. ☐ Since the power does not appear in the original papers, a copy of the power in the prior application is enclosed.
- c. ☒ Recognize as Associate Attorney Jonathan D. Baskin, Reg. No. 39,499.

- d. ☒ Address all future communications to: (May only be completed by applicant, or attorney or agent of record.)

William C. Rowland
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November 15, 1999
Date

By:

Jonathan D. Baskin
Jonathan D. Baskin
Registration No. 39,499

ADDRESS OF
SIGNATOR:

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- ☐ inventor(s)
☐ assignee of complete interest
☒ attorney or agent of record
☐ filed under 37 C.F.R. § 1.34(a)

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Patent Application of)
Xin CHEN et al.) Group Art Unit: Unassigned
Application No.: Divisional of) Examiner: Unassigned
Appln. No. 09/090,918)
Filed: November 15, 1999)
For: PROCESS FOR REMOVING)
UNREACTED AMMONIA FROM AN)
EFFLUENT IN A HYDROCARBON)
AMMOXIDATION REACTION (As)
Amended)

PRELIMINARY AMENDMENT

Assistant Commissioner for Patents
Washington, D.C. 20231

Sir:

Prior to an examination on the merits, please amend the
above-identified application as follows:

IN THE TITLE:

Please delete the title in its entirety, and insert
therefor the following:

--PROCESS FOR REMOVING UNREACTED AMMONIA FROM AN EFFLUENT
IN A HYDROCARBON AMMOXIDATION REACTION--.

IN THE ABSTRACT:

Please delete the abstract, and insert therefor the new abstract on the sheet attached to this paper.

IN THE CLAIMS:

Please cancel Claims 1-4 without prejudice or disclaimer.

Please add new Claims 5-9 as follows:

--5. A process for removing unreacted ammonia from an effluent of a catalyst bed used in a hydrocarbon ammoxidation reaction, comprising the steps of:

(a) providing a fluidized bed reactor, said reactor comprising:

(1) a catalyst bed for reacting ammonia and hydrocarbons therein;

(2) a dilute phase of the catalyst bed disposed above the catalyst bed;

(3) a set of internals disposed at least partially within the dilute phase of the catalyst bed;

(4) an inlet of a first-stage cyclone separator disposed above the set of internals; and

(b) removing the unreacted ammonia from the effluent of the catalyst bed by passing the effluent through

the set of internals, wherein the ammonia and hydrocarbons present in the effluent contact the dilute phase of the catalyst bed and react therein.

6. The process according to Claim 5, wherein the set of internals are selected from the group consisting of packing, baffles, screens and combinations thereof.

7. The process according to Claim 5, wherein a bottom side of the set of internals is at a depth within the catalyst bed of not greater than 20% of the total height of the catalyst bed.

8. The process according to Claim 5, wherein the hydrocarbons are of a compound selected from the group consisting of propane, propylene, isobutene, xylene and combinations thereof.

9. A process for removing unreacted ammonia from an effluent of a catalyst bed used in a hydrocarbon ammoxidation reaction, comprising the steps of:

(a) providing a fluidized bed reactor, said reactor comprising:

(1) a catalyst bed for reacting ammonia and hydrocarbons therein;

(2) a dilute phase of the catalyst bed disposed above the catalyst bed;

(3) a set of internals disposed at least partially within the dilute phase of the catalyst bed; and

(b) removing the unreacted ammonia from the effluent of the catalyst bed by passing the effluent through the set of internals, wherein the ammonia and hydrocarbons present in the effluent contact the dilute phase of the catalyst bed and react therein.--

REMARKS

Entry of the foregoing and examination of the above-identified application, as amended, are respectfully requested.

By the above amendments, Claims 1-4 have been canceled and replaced with new Claims 5-9, directed to processes for removing unreacted ammonia from an effluent of a catalyst bed used in a hydrocarbon ammoxidation reaction. Support for new

Claims 5-9 can be found in the specification at least from page 4, line 18 to page 6, line 19, and at page 8, lines 8-12.

Early and favorable consideration of the application is respectfully requested. If there are any questions concerning this paper or the application in general, the Examiner is invited to telephone the undersigned at the below-listed number.

Respectfully submitted,

BURNS, DOANE, SWECKER & MATHIS, L.L.P.

By: _____

Jonathan D. Baskin

Registration No. 39,499

P.O. Box 1404
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Date: November 15, 1999

ABSTRACT

A process for removing unreacted ammonia from an effluent of a catalyst bed used in a hydrocarbon ammoxidation reaction is provided. The process includes a step of providing a fluidized bed reactor. The reactor includes the catalyst bed for reacting ammonia and hydrocarbons therein. The reactor also includes a dilute phase of the catalyst bed disposed above the catalyst bed. The reactor further includes a set of internals disposed at least partially within the dilute phase of the catalyst bed. The reactor additionally includes an inlet of a first-stage cyclone separator disposed above the set of internals. The process also includes a step of removing the unreacted ammonia from the effluent of the catalyst bed by passing the effluent through the set of internals. The ammonia and hydrocarbons present in the effluent contact the dilute phase of the catalyst bed and react therein.

FPCH981633 (A)

**FLUIDIZED BED REACTOR FOR AMMOXIDATION OF
HYDROCARBONS**

5 This invention relates to a fluidized bed reactor for ammoxidation of hydrocarbons and, more particularly, to a fluidized bed reactor with internals installed in proximity to upper region of the catalyst bed, capable of enhancing the contact efficiency between gas and solid phases.

10 It is an important subject in petrochemical industry to produce unsaturated nitriles by ammoxidation process from hydrocarbons, among which the ammoxidation of propylene and isobutene has long been commercialized for the manufacture of acrylonitrile and methyl acrylonitrile, respectively, and the ammoxidation of paraffinic hydrocarbons has also been under development. A common problem associated with these reactions is due
15 to the fact that unsaturated nitriles are usually unstable and liable to polymerization under basic conditions. For any ammoxidations therefore, it is necessary to eliminate the unreacted ammonia from the product gases. To remove the unreacted ammonia, the prior art has employs a method by sulfuric acid quenching. This method will produce large quantities of nitrile-containing ammonium sulfate waste water, which is difficult to
20 dispose. The strict legislation imposed on pollutant emissions in most countries has rendered the disposal of ammonium sulfate byproduct a critical issue.

Taking the ammoxidation of propylene to acrylonitrile for example, propylene, upon passing through a fluidized bed reactor together with ammonia and air, is ammonia oxidized to form a major product of acrylonitrile and a number of byproducts including
25 acetonitrile, hydrogen cyanide, acrolein, acrylic acid, carbon monoxide and carbon dioxide, as well as small amounts of unreacted propylene and ammonia. After exiting the reactor, the gaseous effluent is cooled and then enters a neutralizing column, where the unreacted ammonia is absorbed by aqueous sulfuric acid to produce ammonium sulfate. At the same time, parts of water vapor are also condensed out, thereby causing the
30 formation of ammonium sulfate waste water. After removing the unreacted ammonia, the gas is introduced into an absorber, where all the organic compounds are absorbed from the gas by low-temperature water. The absorption liquid is then sent to an acrylonitrile recovery and refining unit for the separation of high purity of acrylonitrile, hydrogen cyanide and acetonitrile.

35 In the above described process of acrylonitrile production, it is very important to remove unreacted ammonia with sulfuric acid from the effluent gas in the neutralizing column, because both acrylonitrile and hydrogen cyanide are substances liable to

polymerization, especially in neutral and slightly alkaline conditions. Not only will this cause product loss of acrylonitrile and hydrogen cyanide, but contaminate the equipment and produce ammonium sulfate waste water.

5 The composition of ammonium sulfate waste water is complex, approximately comprising the following groups:

- 10 1. polymers: Because pH value of the circulating spray liquid in the neutralizing column is controlled within the range of 2-7, certain amount of products, such as acrylonitrile, hydrogen cyanide and acrolein, may polymerize to form high polymers. Losses caused by polymerization, calculated based on the total amount of their formation are: acrylonitrile 2-5%, hydrogen cyanide 3-8%, and acrolein up to 40-80%. Therefore the polymer content in the ammonium sulfate waste water is very high. A wider molecular weight distribution is another characteristics of polymers present in the waste water, i.e. some polymers with low molecular weight are soluble in the ammonium sulfate waste water, but other polymers with higher molecular weight will form black solid insoluble in water, thereby leading difficulty in recovering ammonium sulfate.
- 20 2. high boiling components: Since the operation temperature within the neutralizing column is about 80 °C, acrylic acid will be condensed from the effluent gas and present in the ammonium sulfate waste water. Another high boiling component is cyanhydrin, which is formed by the condensation between carbonyl compounds and hydrogen cyanide.
3. low boiling components: mainly acrylonitrile, acetonitrile and hydrogen cyanide etc. dissolved in the ammonium sulfate waste water, their content being normally in the range of 500-5000 ppm, depending on the temperature of spray liquid.
- 25 4. catalyst fine particles: During the production of acrylonitrile in fluidized bed reactor, the major part of catalyst fine particles entrained from the catalyst bed by the product gas is recovered by cyclones and circulated back to the bed. However, small amount of catalyst fines will be blown out of the reactor by the effluent gas and then scrubbed down in the neutralizing column. The catalyst blow-off quantity is about 0.2-0.7 kg per ton of acrylonitrile produced.
- 30

Accordingly, it is very difficult to recover crystalline ammonium sulfate from the ammonium sulfate waste water. Simply burning off the effluents without a prior recovery of ammonium sulfate therefrom will cause secondary pollution owing to the formation of sulfur dioxide, which is not allowed to discharge directly to the atmosphere in most countries. Another problem associated with the disposal of ammonium sulfate waste water by burning method is a combustion temperature as high as 850-1100 °C required to burn out the cyanides from the waste water, thus causing large quantities of fuel consumption. Since sulfur dioxide contained in the combustion flue gas is corrosive to

steel material, the use of waste heat boilers for recovering the heat energy is limited. Moreover, direct vent of high temperature flue gas will cause thermal pollution to the atmospheric environment.

In summary, the formation of ammonium sulfate in the production of acrylonitrile leads to a severe problem, which has severely limited further development of the acrylonitrile manufacture industry. Therefore development of a clean process for the production of acrylonitrile which produce no ammonium sulfate has become the concerned focus in the art worldwide. The key point of this clean process is to maximize ammonia conversion during the production in order to eliminate the unreacted ammonia.

Elimination of unreacted ammonia can be achieved by two ways: one starts with the catalyst to increase ammonia conversion of the catalyst; the other starts with the ammoxidation reaction to enable ammoxidation of propylene and elimination of unreacted ammonia to proceed separately.

Further increasing ammonia conversion of the propylene ammoxidation catalyst can be difficult to achieve. To take account of ammoxidation only, the catalyst is required to have lower ability to decompose ammonia, i.e. to yield higher acrylonitrile yield while using a lower feed ratio of propylene to ammonia. If the catalyst has a higher decomposition ability for ammonia, the increase of ammonia consumption will render it uneconomic. Therefore these two requirements are contradictory. Since ammonia conversion of the current catalyst is very low, to increase ammonia conversion of the catalyst to certain level without increasing the ammonia consumption still deserves attention. Because certain amount of acrylic acid is also formed during propylene ammoxidation, it is not necessary to increase ammonia conversion of the catalyst to as high as 100%. For a conversion up to 97—98%, it may not need essentially to add sulfuric acid for neutralization. For example, Chinese Patent 96116456.5 is an example in an effort to increase ammonia conversion of the catalyst. From the viewpoint of extended stable operation of the plant, the inventor believes that there should be other measures to attain complete elimination of the unreacted ammonia. This is because of the fact that the ability of a catalyst to decompose ammonia is related to how long it has been used, and also influenced by the operating conditions of the reactor, which cannot be maintained unchanged for long periods of time.

To eliminate the unreacted ammonia by virtue of the secondary reaction of propylene ammoxidation is a useful method and has been disclosed in patents. U.S. Patent Nos. 5,457,223 and 5,466,857, Japanese Patent No. 96-27087 and WO 9625391 disclose that methanol, acetonitrile and other oxidable organic compounds, introduced into the dilute phase at the upper region of a fluidized bed reactor where propylene is ammonia-oxidized with molybdenum-bismuth-iron system catalyst to synthesize acrylonitrile, may react with ammonia therein to form hydrogen cyanide and eliminate ammonia. At the optimum

conditions, ammonia can be reacted completely. This method, however, suffers from the oxygen depletion problem at the dilute phase of the reactor where oxygen is needed for ammonia to react with organic compounds, and the catalyst will therefore be over-reduced. As a result, the single-pass yield of acrylonitrile will decrease, and the catalyst stability may be affected as well.

WO 9623766 discloses another method by adjusting the molar ratio of the feed to the reactor to keep the molar ratio of the organic acids formed such as acrylic acid etc. to the unreacted ammonia in the range of 0.8—3.0. In this case, the unreacted ammonia will subsequently combine with the organic acids to form the corresponding ammonium salts, thereby eliminating the need of sulfuric acid. The disadvantage of this method is the formation of unsaturated carbonyl compounds in large amounts along with the formation of organic acids. This will cause difficulty for the recovery and refining of acrylonitrile, as well as decrease its single-pass yield.

The inventor has identified, through a consistent and thorough review of the full range of fundamental processes in acrylonitrile synthesis at a fluidized bed reactor, that the unreacted ammonia may be eliminated by resorting the secondary reaction of propylene ammoxidation, even without the addition of any oxidable organic compounds.

To overcome these and other deficiencies of the prior art it is therefore an object of the present invention to provide a fluidized bed reactor for ammoxidation of hydrocarbons, which contains a set of suitable internals installed in proximity to the upper region of the catalyst bed, capable of enhancing the contact efficiency between gases and solids therein, and serves the function of increasing the ammonia conversion, thereby decreasing the content of unreacted ammonia in the effluent gas.

The above mentioned internals include packings, baffles and screens etc. Said internals help to bring about more uniform mixing between the reactive gas leaving the catalyst bed and the catalyst entrained by the gas flow in the space above the catalyst bed, thus increasing the contact efficiency between gas and catalyst particles, which will be beneficial to the further reaction occurring within the dilute phase zone and elimination of the unreacted ammonia from the effluent gas.

Within the reactor the internals are positioned, for baffles or screens, with their bottom plate (screen) beneath the surface of the catalyst to keep its depth not beyond 20% of the height of the fluidized bed, while with their top side not beyond the inlet of the first-stage cyclone separator, preferably at the level of the dust hopper of the cyclone separator. For packings, the positions of their top and bottom side within the reactor are the same as said above.

The packings used are made of screens generally limited to 10 mesh or more, in the form of circular, cylindrical, square, rectangular, honeycomb and the like, and with a void factor (fractional free area) in the range of 20—80%, preferably in the range of 35—

60%. The packings may be packed within the reactor either randomly or regularly. Special method can also be used, for example, to fix the packings by springs so as to enable it to vibrate under the action of product gas flow to prevent their surfaces from catalyst deposition.

5 The baffles or screens used include perforated grid plates, perforated plates, perforated plates with cone or pyramid cap or louver plates etc. Their openings may have different geometries, such as rectangular, triangular, circular, elliptical etc. with a void factor (fractional free area) in the range of 20—80%, preferably in the range of 35—65%. The baffles or screens may be placed horizontally or at a certain slope. For inclined
10 arrangement, the slope angle must be greater than the angle of repose of the catalyst to prevent catalyst accumulation over its surface. The spacing L between various layers of baffles or screens may be identical or different, depending on the inside diameter of the reactor (D). L/D may vary from 0.2 to 2.0.

At the upper region of the catalyst bed of the fluidized bed reactor ammonia
15 undergoes secondary reaction, accompanied by heat generation. Accordingly, the ammonia conversion of the catalyst should not be too low, to prevent temperature at the reactor top from going too high. In this invention, the ammonia conversion is required above 85%, preferably above 93%. All olefine ammoxidation catalysts, more preferably catalysts with molybdenum oxide as the major component are applicable to this invention,
20 such as the catalyst described in Chinese Patent CN1021638C. A catalyst of higher ammonia conversion is more preferred.

Gas superficial velocity within the fluidized bed reactor bears a relation to the catalyst concentration at the dilute phase of the reactor top. It should be in the range of 0.5—0.8 m/s, preferably in the range of 0.6—0.75 m/s. The temperature at the upper
25 reactor should be the same as or close to the temperature of catalyst bed. The reaction pressure depends on the activity of the catalyst used, normally in the range of 0.05—0.2 MPa.

This invention is the main part of an overall acrylonitrile manufacture process which can minimize ammonium sulfate formation or produce no ammonium sulfate. After
30 propylene, ammonia and air pass through the fluidized bed reactor of the invention, the product gas is cooled and enters a quenching column for further cooling, then is sent into a scrubber, where all organic matters are absorbed from the gas by low-temperature water. The absorption liquid is passed to an extraction column, where water is used as a solvent to separate acrylonitrile from acetonitrile. Raw acrylonitrile overhead out of the column
35 contains hydrogen cyanide and small amount of water. It then passes through a column to remove hydrogen cyanide and a dewatering column, thereby obtaining acrylonitrile product of high purity.

The present invention uses the secondary reaction taking place within the dilute

phase of the fluidized bed reactor to remove unreacted ammonia from the product gas, but it adds no organic compounds at all. The effluent gas leaving the catalyst bed contains, in addition of acrylonitrile and byproducts such as acetonitrile, hydrogen cyanide, acrolein, acrylic acid, carbon monoxide, carbon dioxide etc., small amount of unreacted propylene and ammonia, which contact with the catalyst present at the dilute phase of the fluidized bed for further reaction. The unreacted ammonia reacts with acrolein byproduct and residual propylene to form acrylonitrile, thereby increasing the acrylonitrile production and decreasing the acrolein content. It therefore has an advantage.

Since the effluent gas leaving the catalyst bed does not rise uniformly, and the internals installed at the dilute phase of the fluidized bed are available to bring about more uniform mixing between the gas and the catalyst and increase the contact efficiency therebetween, the ammonia conversion is thus increased to enable the content of unreacted ammonia to be decreased and good results to achieve. The fluidized bed reactor of this invention is applicable to the ammoxidation of propane, propylene, isobutene and xylene, not only for the retrofitting of existing facilities, but for the developing of new processes. For ammoxidation process, this invention can intensify productivity, increase reaction efficiency, simplify the process flowsheet, decrease pollution to the environment, and thus yield greater economy. The invention will be further illustrated by the following examples.

Comparative Example 1

A catalyst of the same composition as in Example 1 of CN 102163C was used. The fluidized bed reactor was 38 mm in inside diameter and about 2 m tall. 550 g of catalyst were added with a catalyst bed height of 320 mm. The reaction temperature was 435 °C, reaction pressure 0.08 MPa, the feed ratio was propylene : ammonia : air = 1 : 1.2 : 9.8, and the feed rate of the gas mixture was 4.3 L/min. The reaction result indicated a propylene conversion of 96.2%, acrylonitrile single-pass yield of 80.1%, acrylonitrile selectivity of 83.3%, and ammonia conversion of 93%.

Example 1

The same condition was followed as in Comparative Example 1 except that 5 perforated plates were placed at the reactor top with the height of the first plate from the gas distributor as 300 mm, and the heights of other four plates as 350, 400, 450 and 500 mm, respectively. The holes were 4 mm in diameter and the fraction of plate consisting of free area was 40%. The reaction result showed a propylene conversion of 98.5%, acrylonitrile single-pass yield of 81.7%, acrylonitrile selectivity of 82.9%, and ammonia conversion of 96.2%.

Example 2

The same condition was used as in Example 1 except that 3 identical perforated

plates were placed with the first plate at the same height as in Example 1 and the heights of the 2nd and 3rd plates as 400 and 500 mm, respectively. The reaction result showed a propylene conversion of 97.8%, acrylonitrile single-pass yield of 81.2%, acrylonitrile selectivity of 83.0%, and ammonia conversion of 95.5%.

5 Example 3

The same condition was used as in Example 1 except that 8 identical perforated plates were placed with the first plate at the same height as in Example 1 and a plate spacing of 30 mm. The reaction result showed a propylene conversion of 98.8%, acrylonitrile single-pass yield of 81.7%, acrylonitrile selectivity of 82.7%, and ammonia conversion of 96.5%.

10 Example 4

The same condition was used as in Example 2 (i.e. adding 3 perforated plates) except that the catalyst amount was 750 g and the feed rate of gas mixture was increased to 6 L/min. The reaction result showed a propylene conversion of 98.7%, acrylonitrile single-pass yield of 81.8%, acrylonitrile selectivity of 82.9%, and ammonia conversion of 97.5%.

15 Example 5

The same condition was used as in Example 1 except that within the reactor were placed cylindrical packings made of 10 mesh×6 mm stainless steel screens. The height of packings bottom from the gas distributor was 300 mm and its length 200 mm. The reaction result showed a propylene conversion of 98.8, acrylonitrile single-pass yield of 81.4%, acrylonitrile selectivity of 82.4%, and ammonia conversion of 97.2%.

It can be seen from the Example mentioned above:

- 25 1. For the fluidized bed reactor with the internals comprising packings or baffles according to the invention, the ammonia conversion is increased by 4-5% with acrylonitrile single-pass yield and acrylonitrile selectivity keeping fixed.
2. Increasing the number of baffles (screens) or the height of packings as well as properly raising the feed rate of the gas result in better ammonia conversion.

What is claimed is :

1. A fluidized bed reactor for the ammoxidation of hydrocarbons, which is characterized by installing a set of internals in proximity to upper region of the catalyst bed, capable of enhancing the contact efficiency between gas and solid phases.
2. The fluidized bed reactor for the ammoxidation of hydrocarbons according to claim 1 wherein said internals comprise packings, baffles, screens, and the like.
3. The fluidized bed reactor for the ammoxidation of hydrocarbons according to claim 1 wherein said internals are positioned with their bottom side beneath the surface of the catalyst bed to keep its depth not larger than 20% of the height of said fluidized bed, while with their top side not beyond the inlet of the first-stage cyclone separator.
4. The fluidized bed reactor for the ammoxidation of hydrocarbons according to claim 1 wherein said hydrocarbons are propane, propylene, isobutene or xylene.

FLUIDIZED BED REACTOR FOR AMMOXIDATION OF HYDROCARBONS

ABSTRACT

5 This invention relates to a fluidized bed reactor for ammoxidation of hydrocarbons,
with internals installed within the fluidized bed, capable of enhancing the contact
efficiency between gas and solid phases and comprising packings, baffles, louver plates,
screens and the like. Said fluidized bed reactor of this invention offers a convenient
approach to increase the ammonia conversion and may be used in commercial
10 applications.

**COMBINED DECLARATION AND POWER OF ATTORNEY
FOR UTILITY PATENT APPLICATION**

Attorney's Docket No.
006005-019

As a below-named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name;

I BELIEVE I AM THE ORIGINAL, FIRST AND SOLE INVENTOR (if only one name is listed below) OR AN ORIGINAL, FIRST AND JOINT INVENTOR (if more than one name is listed below) OF THE SUBJECT MATTER WHICH IS CLAIMED AND FOR WHICH A PATENT IS SOUGHT ON THE INVENTION ENTITLED:

FLUIDIZED BED REACTOR FOR AMMOXIDATION OF HYDROCARBONS

the specification of which

(check one)

☐ is attached hereto;

☒ was filed on June 5, 1998 as

Application No. _____

and was amended on _____;
(if applicable)

I HAVE REVIEWED AND UNDERSTAND THE CONTENTS OF THE ABOVE-IDENTIFIED SPECIFICATION, INCLUDING THE CLAIMS, AS AMENDED BY ANY AMENDMENT REFERRED TO ABOVE;

I ACKNOWLEDGE THE DUTY TO DISCLOSE TO THE OFFICE ALL INFORMATION KNOWN TO ME TO BE MATERIAL TO PATENTABILITY AS DEFINED IN TITLE 37, CODE OF FEDERAL REGULATIONS, Sec. 1.56 (as amended effective March 16, 1992);

I do not know and do not believe the said invention was ever known or used in the United States of America before my or our invention thereof, or patented or described in any printed publication in any country before my or our invention thereof or more than one year prior to said application; that said invention was not in public use or on sale in the United States of America more than one year prior to said application; that said invention has not been patented or made the subject of an inventor's certificate issued before the date of said application in any country foreign to the United States of America on any application filed by me or my legal representatives or assigns more than twelve months prior to said application;

I hereby claim foreign priority benefits under Title 35, United States Code Sec. 119 and/or Sec. 365 of any foreign application(s) for patent or inventor's certificate as indicated below and have also identified below any foreign application for patent or inventor's certificate on this invention having a filing date before that of the application(s) on which priority is claimed:

COMBINED DECLARATION AND POWER OF ATTORNEY

Attorney's Docket No.
006005-019

COUNTRY/INTERNATIONAL	APPLICATION NUMBER	DATE OF FILING (day, month, year)	PRIORITY CLAIMED
CHINA	CN97106455.5	6 June 1997	YES <input checked="" type="checkbox"/> NO <input type="checkbox"/>
			YES <input type="checkbox"/> NO <input type="checkbox"/>

I hereby appoint the following attorneys and agent(s) to prosecute said application and to transact all business in the Patent and Trademark Office connected therewith and to file, prosecute and to transact all business in connection with international applications directed to said invention:

William L. Mathis	17,337	Robert G. Mukai	28,531	William H. Benz	25,952
Peter H. Smolke	15,913	George A. Hovanec, Jr.	28,223	Peter K. Skiff	31,917
Robert S. Swecker	19,885	James A. LaBarre	28,632	Richard J. McGrath	29,195
Piston N. Mandros	22,124	E. Joseph Gess	28,510	Matthew L. Schneider	32,814
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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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